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Thermodynamic Modelling of Waste to Energy Power Plant: A Case Study in Makassar City, Indonesia

Abstract. Waste is a major problem in big cities in Indonesia, one of which is Makassar City. Every year the amount of waste generated by the residents of Makassar City continues to increase, but this is not proportional to the capacity of the landfill. Therefore, researchers want to design a waste-to-energy power plant system in Makassar City or other words apply the waste-to-energy concept. The waste-to-energy concept aims to process waste into energy and reduce the volume of waste in landfills. Then the research method used is thermodynamic modelling using STEAG Ebsilon Professional version 13.02 software. From this analysis it was found that the capacity of the waste that can be burned is 742.648 tons/day, the thermal input of the incinerator is 39.011 MW, the thermal capacity of the boiler is 30.749 MW, the thermal efficiency of the waste-to-energy boiler with direct method 83.123 % and with indirect method 82.107 %, the mechanical power of the steam turbine is 10.816 MW, the heat duty of the high-pressure feed-water heater is 1,681.321 kW, the heat duty of the low-pressure feed-water heater is 1,681.321 kW, the heat duty of the low-pressure feed-water heater is 1,681.321 kW, an at thermal efficiency of 24.110%, a gross plant heat rate of 12,683.130 kJ/kg, a net plant heat rate of 13,816.942 kJ/kg, an auxiliary load of 912.744 kW, a net plant power of 9.638 MWe, the specific fuel consumption 1.124 kg/kWh for each unit at the maximum load, and reducing municipal solid waste generation per year by 271,066.520 tons.

Streszczenie. Odpady stanowią poważny problem w dużych miastach Indonezji, jednym z nich jest Makassar City. Każdego roku ilość odpadów wytwarzanych przez mieszkańców Makassar City stale rośnie, jednak nie jest to proporcjonalne do pojemności składowiska. Dlatego badacze chcą zaprojektować system elektrowni przetwarzających odpady na energię w mieście Makassar, czyli innymi słowy zastosować koncepcję przetwarzania odpadów na energię. Koncepcja waste-to-energy ma na celu przetwarzanie odpadów na energię i zmniejszenie ilości odpadów trafiających na składowiska. Następnie zastosowaną metodą badawczą jest modelowanie termodynamiczne z wykorzystaniem programu STEAG Ebsilon Professional wersja 13.02. Z analizy tej wynika, że wydajność spalania odpadów możliwych do spalenia wynosi 742,648 ton/dobę, moc cieplna spalarni wynosi 39,011 MW, moc cieplna kotła wynosi 30,749 MW, sprawność cieplna spalarni -kocioł energetyczny metodą bezpośrednią 82,123 % i metodą pośrednią 82,107 %, moc mechaniczna turbiny parowej 10,816 MW, obciążenie cieplne wysokociśnieniowego podgrzewacza wody zasilającej 1681,321 kW, obciążenie cieplne niskociśnieniowego Moc podgrzewacza wody zasilającej wynosi 1780,234 kW, a wydajność chłodnicza skraplacza chłodzonego powietrzem 20,337 MW. Konstrukcja ta charakteryzuje się sprawnością cieplną netto wynoszącą 24,110%, współczynnikiem ciepła brutto instalacji wynoszącym 912,744 kW, mocą netto instalacji wynoszącą 9,638 MWe, zużycie paliwa 1,124 kg/kWh na każdą jednotkę przy maksymalnym obciążeniu oraz ograniczenie wytwarzania odpadów komunalnych w skali roku o 271 066,520 ton. (Modelowanie termodynamiczne elektrowni przetwarzającej odpady na energię: studium przypadku w mieście Makassar w Indonezji)

Keywords: Thermodynamic-Modelling, Municipal Solid Waste, Power Plant **Słowa kluczowe**: Modelowanie termodynamiczne, odpady komunalne, elektrownia

Introduction

So far, boiler heat energy sources use fossil fuels, while alternative energy sources that can be considered are waste energy sources and renewable energy sources.[1]. One part of waste energy is Municipal solid waste (MSW). MSW is a term usually applied to a heterogeneous collection of wastes produced in urban areas. Generally, urban wastes can be subdivided into two major components: organic and inorganic. The characteristics and quantity of the solid waste generated in a region are a function of the standard of living in the city or country. Wastes generated in developing countries have a large proportion of organic waste, while the wastes in developed countries are more diversified with relatively larger shares of plastics and paper [2]. Almost all economic sectors generate municipal solid waste. Some factors that influence high MSW generation are population and economic growth, education, occupation, consumption patterns, and gross domestic product per capita. With a high gross domestic product,

Indonesia generates large amount of annual municipal solid waste (SW) in ASEAN countries [3]. The annual production of municipal solid waste in Indonesia reaches 31 million tons with the waste composition including food waste at 39.23%, plastic at 18.11%, paper at 12.83%, wood at 12.16%, metal at 3.19%, cloth at 2.55%, glass 2.42%, leather 1.82%, and others 7.69% [4]. Meanwhile, Makassar City's annual solid waste production reaches 1,023,710 tons with a composition of food waste at 54.70%, wood at 11.33%, plastic at 12.20%, paper at 6.78%, textile at 1.30%,

glass at 1.15%, metal 1.07%, battery 0.62%, rubber 0.42% and other 10.43% [5]. Indonesian municipal solid waste has a high moisture content, volatile matter content, as well as carbon and hydrogen content, and contains more organic matter. Moisture content is a major factor impacting calorific value. The lower heating value on the wet basis of the entire municipal solid waste sample is 8.6 MJ/kg, which is not only relatively high compared with the average calorific value, but also above the World Bank-recommended calorific value minimum for waste-to-energy applications. Thermal conversion processes including incineration, pyrolysis, and gasification for heat, bio-oil, and syngas generation are already well established and are being employed in several countries [6] . MSW in Indonesia is for waste-to-energy, suitable whether combustion (incineration) or gasification-based [7].

The concept of waste-to-energy aims to process waste into energy and reduce the volume of waste in landfills. The most commonly used technology for converting waste into energy is incineration [8]. This is because incineration technology provides a more productive way of de-creasing the amount of urban solid waste that needs to be landfilled. The incineration of municipal solid waste can minimize its mass by 70% and volume by 90%, as well as electricity and heat recovery [9]. The purpose of this research is to get a waste-to-energy power plant model that is suitable and can solve the waste problems in Makassar City.

Fuel from waste

Makassar City has a daily potential power from the waste of 24.882-33.768 MWe with an LHV variation of 7-8.6 MJ/kg and an average amount of waste of 1,023,710 tons/day in 2021. Makassar City municipal solid waste production data is shown in Table 1.

Table 1. Makassar City municipal solid waste production data [5].

Year	Daily (tons/day)	Yearly	
		(tons/year)	
2008	386.826	141,191.49	
2009	456.318	166,556.07	
2010	532.744	194,451.56	
2011	529.878	193,405.47	
2008	386.826	141,191.49	
2012	557.312	203,418.88	
2013	676.632	246,970.68	
2014	677.213	247,182.75	
2015	674.716	246,271.34	
2016	651.649	237,851.89	
2017	795.129	290,222.09	
2018	707.923	258,391.90	
2019	696.585	254,253.53	
2020	996.71	363,799.15	
2021	1,023.71	373,654.15	
Total	9,363.35	3,417,620.93	

Waste to energy power plant description

The Makassar City waste-to-energy power plant model consists of two identical units. Each of the two waste-toenergy power plant units has a high-pressure feedwater heater, a low-pressure feedwater, a deaerator, a steam turbine, an electric generator, a boiler, and four air-cooled condenser units. The estimated incinerator capacity of this power plant is 842.7 tons per day with an estimated power that can be generated of 20,482 – 25,164 MWe. The technical data of the Makassar City waste-to-energy power plant model is shown in Table 2.

Table 1 Combustion parameters [10, 11]				
Minimum combustion temperature (°C)	850			
Maximum combustion temperature (°C)	1450			
Primary combustion zone air ratio	<1.2			
Secondary combustion zone air ratio	1.7			
Table 3 Steam and water cycle parameters [12]				
Economizer working pressure (bar)	93.342			
Evaporator working pressure (bar)	93.342			
Superheater working pressure (bar)	90.623			
Economizer working temperature (°C)	250			
Evaporator working temperature (°C)	305.974			
Superheater working temperature (°C)	449			
Economizer pressure drop (bar)	7.468			
Evaporator pressure drop (bar)	14			
Superheater pressure drop (bar)	0.020			
Table 2 Boiler Ratings [8],				
Air ratio	1.2			
Circulation ratio	5			
Air Fuel Ratio for LHV 8.6 MJ/kg	3.409			
Flue gas recirculation ratio (%)	15			
Table 3 Steam turbine parameters [13, 14]				
Steam turbine type	Siemens			
,, , , , , , , , , , , , , , , , , , ,	SST-200			
h ₁ (kJ/kg), with T=447.464 °C and P=88 bar	3,254.308			
h ₂ (kJ/kg), with T=337.839 °C and P=40 ba	r 3,062.643			
h_3 (kJ/kg), with T=337,839 °C and P=40 bar	3,062.643			
h ₄ (kJ/kg), with T=231,363 °C and P=16 bar	2,874.053			
h ₅ (kJ/kg), with T=231.363 °C and P=16 bar	2,874.053			
h ₆ (kJ/kg), with T=170.414 °C and P=8 bar	2,751.521			
h ₇ , (kJ/kg), with T=170.414 °C and P=88 ba				
h ₈ (kJ/kg), with T=60.059 °C and P=0.2 ba	r 2,249.696			
Isentropic efficiency (%)	88.0			
$\mathbf{M}_{\mathbf{r}}$	00.0			

Mechanical efficiency (%)

Steam turbine speed (rpm)	7,300
Gearbox speed (rpm)	3,000
Controlled extraction	Up to 4
Condensing pressure for air-cooled condenser (bar abs)	0.2

Modelling and simulation of wate to energy power plant

The modelling process was carried out by entering the technical data of the waste power plant into the model as shown in Fig. 1. The simulation process was performed to determine the performance of the model at the maximum load of each unit, which is 10.5 MWe. The performance observed in the model is the amount that can be burned, the thermal capacity of the boiler, the mechanical power of the steam turbine, the heat duty of the high-pressure feedwater heater, the heat duty of the low-pressure feedwater heater, the cooling duty of the air-cooled condenser, net thermal efficiency, net plant heat rate, auxiliary load, net plant power, and specific fuel consumption.

The equation used to calculate the net thermal efficiency of the model is as follows [15]:

(1)
$$\eta_{th} = \frac{3,598 \, (kJ)}{\text{Net plant heat rate} \left(\frac{kJ}{kWh}\right)}$$

The equation used to calculate the net plant heat rate is as follows [15]

(2)
$$NPHR = \frac{(\hat{m}_{fuel} \times LHV) \, 3,598 \, (kJ)}{(Gross \, power \, (kW) - Auxiliary \, power \, (kW))}$$

The equation used to calculate specific fuel consumption is as follows ([15]:

(3)
$$SFC = \frac{Net \ plant \ heat \ rate\left(\frac{kj}{kwh}\right)}{LHV\left(\frac{kj}{kg}\right)}$$

Result and discussion

After conducting a simulation of the waste power plant model as shown in Fig. 1, the researchers got the results for each unit shown in Table 6.

Table 4	Simulation	results	of	the	waste-to-energy	power	plant
model for	r each unit.					-	-

tem
28.384
26.055
12,638.130
13,816.942
1.214
10,500.000
9,638.375
861.625
8.6
13,816.942
1.214
10,500.000
9,638.375
861.625
8.6
83.123
82.107
4,330.937
371.324
52.745
1,363.416
39,011.862
3,855.444
20,481.517
6,412.241

98.0

Air preheater heat load (kW)	2,186.724			
Useful heat (kW)	30,749.203			
Exhaust losses (kW)	4,656.612			
Slag losses (kW)	1,891.010			
Radiation losses (kW)	153.523			
Uncountable losses (kW)	1,561.514			
Total heat losses (kW)	8,262.659			
Maximum acid dew point (°C)	157.345			
Slag (ton/day)	143.098			
Fly ash (ton/day)	12.273			
Steam turbine				
Inlet mass flow rate (kg/s)	12.401			
Extraction 1 mass flow rate (kg/s)	2.076			
Extraction 2 mass flow rate (kg/s)	0.647			
Exhaust stage mass flow rate (kg/s)	9.679			
Gross mechanical power (MW)	10,816.267			
Net mechanical power (MW)	10,652.328			
Transmission losses (MW)	98.484			
Transmission efficiency (%)	163.938			
High-pressure feedwater heater				
Hot side mass flow rate (kg/s)	0.585			
Cold side mass flow rate (kg/s)	12.041			
Heat duty (kW)	1,681.321			
Heat load (kW)	815.165			
Low-pressure feedwater heater				
Hot side mass flow rate (kg/s)	0.647			
Cold side mass flow rate (kg/s)	10.326			
Heat duty (kW)	1,780.234			
Heat load (kW)	895.898			
Air-cooled condenser				
Hot side mass flow rate (kg/s)	10.326			
Cold side mass flow rate (kg/s)	791.957			
Cold side outlet temperature (°C)	58.042			
Heat load (MW)	22,658.250			
Cooling duty (MW)	20,337.237			
Total required power for fans (kW)	236.600			
Electric generator				
Real power (MW)	10.500			
Idle power (MVAR)	5.085			
Apparent power (MVA)	11.666			

Waste to Energy Power Plant Efficiency

From the simulation results, it can be seen that the net thermal efficiency of the waste-to-energy power plant system model is 24.110%. These results are following research conducted by Mutz [16], which states that in general the thermal efficiency of waste-to-energy power plants is 20% this is in line with research conducted by Branchini [8], which states that in general the thermal efficiency of waste power plants ranges from 18% to 25% and in some cases more than 30%.

In addition, the model of the waste power plant system created by the researchers also uses a low air ratio to increase the net thermal efficiency of the waste power plant. This is in line with research conducted by Gablinge [11] which states that another benefit of using a low air ratio in a waste power plant is an increase in thermal efficiency.

Waste to Energy Boiler Efficiency

From the simulation results, it can be seen that the boiler thermal efficiency obtained is 83.123 % with the direct method and 82.107 % with the indirect method. These results are equal to the results of research conducted by Schu and Leithner [17], which state that the efficiency of the thermal waste-to-energy boiler is around 83%.

System Heat Balance

From the simulation results, it can be seen that the model of the waste-to-energy power plant system experiences the greatest heat losses in the air-cooled condenser and stack. The Sankey diagram of the model of the waste-to-energy power plant system can be seen in Fig. 2. The heat losses that occur in the air-cooled condenser are 20.337 MW or 50.237 % of the system. This happens because all the steam that has been used by the steam turbine and closed feedwater heater flows into the watercooled condenser to change the phase from steam to water by removing the latent heat from the steam. So that the steam that has changed phase to water can flow back to the boiler. The heat losses that occur in the stack (exhaust losses) are 4.656 MW or 15.114 %. This is due to the temperature of the flue gas released into the atmosphere through the stack is high, which is 160 °C which then causes a lot of heat to be wasted from the flue gas.

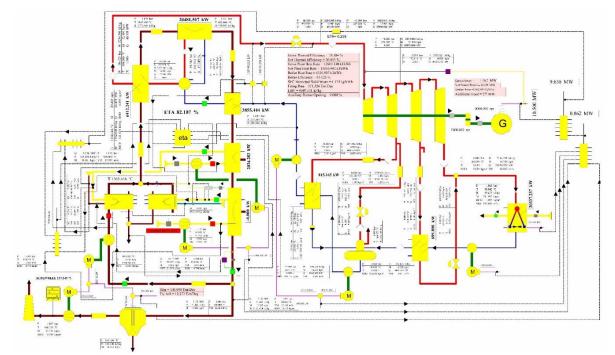


Fig.1. An example of the figure inserted into the text Model of waste-to-energy power plant system using STEAG Ebsilon Professional

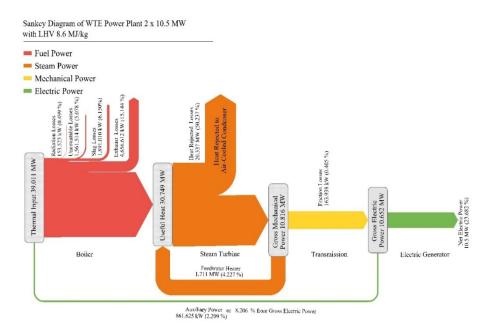


Fig. 2. Sankey diagram from the model of waste-to-energy power plant system.

Conclusion

The thermodynamic modelling using STEAG Ebsilon Professional software version 13.02 was presented. The model of the waste-to-energy power plant for Makassar City has an incinerator daily capacity of 371.323 ton/day at the maximum load of 10.5 MWe for each unit, the thermal capacity of the waste-to-energy boiler is 30,749 MW, the thermal efficiency of the waste-to-energy boiler is 83.123 %, the thermal efficiency of the waste-to-energy boiler, the mechanical power of the steam turbine is 10.816 MW, the heat duty of the high-pressure feedwater heater is 1,681.321 kW, the heat duty of the low-pressure feedwater heater is 1,780.234 kW, and the cooling duty of the aircooled condenser 20.337 MW, the net thermal efficiency is 26.055%, the net plant heat rate is 13.816.942 kJ/kWh, the auxiliary load is 912.744 kW, a net plant power of 9.638 MWe, the specific fuel consumption is 1.124 kg/kWh with LHV 8.6 MJ/kg. This waste-to-energy power plant model is suitable to be implemented and can solve waste problems in Makassar City.

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